


**WESTCARB Annual Business Meeting**

**CO<sub>2</sub> Storage in Natural Gas Reservoirs: Significance of the Rosetta Resources Pilot**



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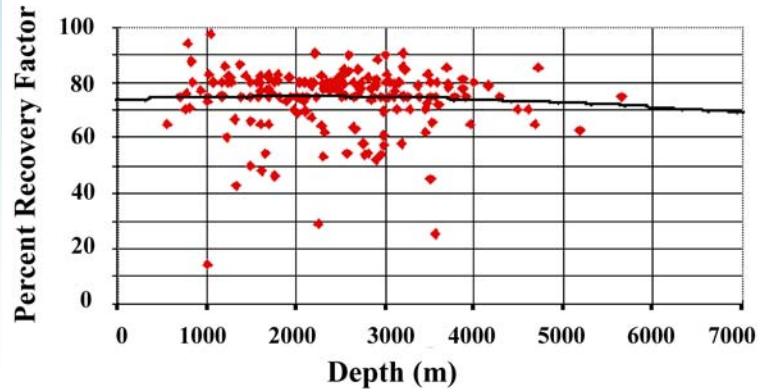
## Outline

- Carbon Sequestration with Enhanced Gas Recovery (CSEGR)
  - Opportunity
  - Concept and its history
  - Technical feasibility
  - Benefits and challenges of CSEGR
- Three pilots world-wide on CSEGR
  - K12B, Netherlands
  - Otway Basin, Australia
  - Rosetta Resources, California
- Results from Rosetta Resources CSEGR Pilot will be of world-wide interest



## CSEGR Opportunity

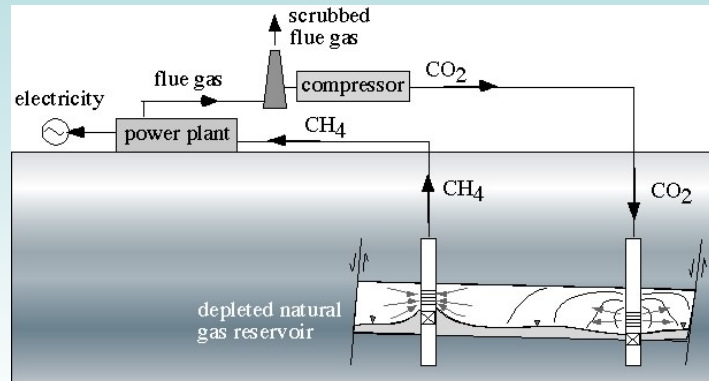
World outside N. America: recovery factor of non-associated gas fields (> 1 Tcf) versus depth



Source: Laherrère (<http://www.hubbertpeak.com/laherrere/iea1997/>)



## CSEGR Concept and History



**Early papers:**

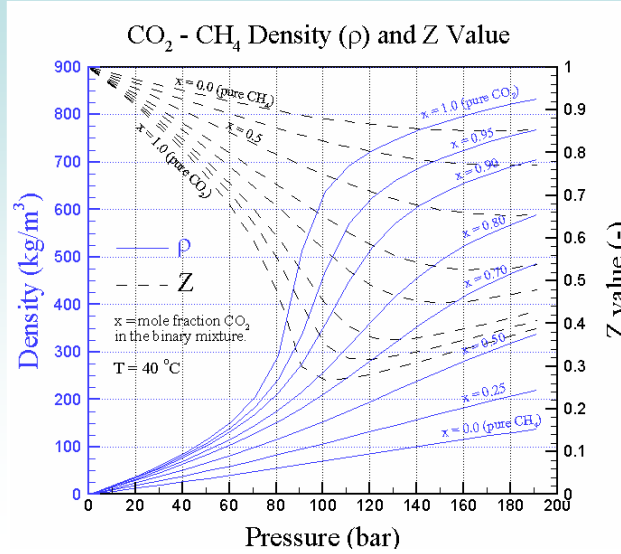
Van der Burgt, Cattle, and Boutkan, *Energy Conv. & Mgt.*, 33(5-8), 603-610, 1992.

Blok, Williams, Katofsky, and Hendriks, *Energy*, 22(2-3), 161-168, 1997.

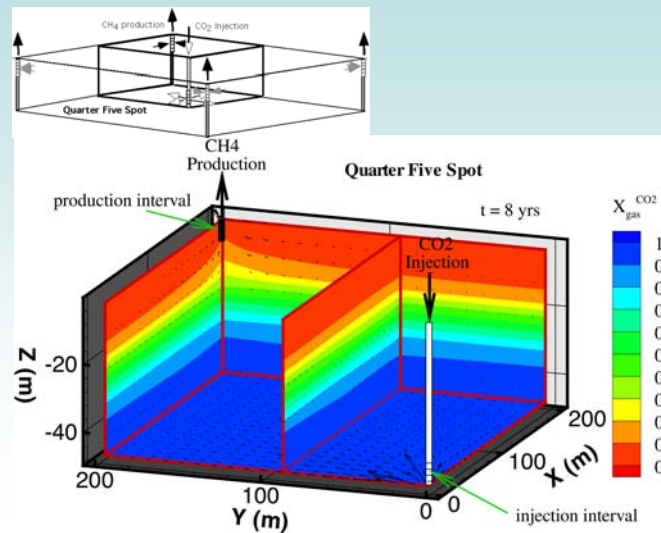
Oldenburg, Pruess, and Benson, *Energy & Fuels*, 15(2), 293-298, 2001.



## Density Contrast Is the Key to CSEGR



## Technical Feasibility



Oldenburg, Stevens, and Benson, *Energy* 29, 1413-1422, 2004.

## CO<sub>2</sub> in Depleted Gas Reservoirs

### Benefits

- Maintain/increase reservoir pressure.
  - Decrease water entry
  - Avoid subsidence
- Enhance/accelerate/control methane recovery
  - Primary gas recoveries approx.:
    - 80-90% for depletion drive
    - 60-70% for water drive
- Utilize idled wells (for production and injection).
- Develop value of depleted reservoirs as CO<sub>2</sub> storage sites.
- Use CO<sub>2</sub> as cushion gas for natural gas storage.
- Promote new technologies against global warming.
- Join new industry of geologic CO<sub>2</sub> storage.



## Key Issues for CSEGR

### Challenges

- Early breakthrough
- Mixing of CO<sub>2</sub> and CH<sub>4</sub> that degrades gas quality
- Injectivity decline due to halite precipitation
- Pressurization due to mixing
- Joule-Thomson cooling (hydrate formation)



## CO<sub>2</sub> Projects Related to Gas Reservoirs

Name	Country	Organizations	Status	Environ.	Depth	Storage	CO <sub>2</sub> Injection	CO <sub>2</sub> source
K12B	Netherlands	Gaz de France	Operating	Offshore	4000 m	EGR	30,000 up to 475,000 t/yr	Natural gas
Rosetta	U.S. (Calif.)	Rosetta Resour., WESTCARB	2007 pilot	Onshore	1000 m	EGR	500 t	Commercial
Otway	Australia	CO2CRC	2007 pilot	Onshore	2000 m	EGR (water leg)	100,000 t	Natural gas
Altmark	Germany	BGR	Under evaluation	Onshore	3000 m	EGR	Unknown	Various
Atzbach, Schwinst.	Austria	Rohoel	Under evaluation	Onshore	1600 m	EGR	200,000 t/yr	Various
Ketzin	Germany	GFZ	Experimental site	Onshore	700 m	Exptl.	< 10,000 t/yr	Commercial
In Salah	Algeria	BP, Statoil, Sonatrach	Operating > July 2005	Onshore	1900 m	Water leg	> 1 Mt/yr	Natural gas
Gorgon	Australia	Chevron	Pending approval	Onshore (Barrow Is.)	2300 m	Aquifer	3 Mt/yr	Natural gas
Snohvit	Norway	Statoil	2007	Offshore	2500 m	Aquifer below	750,000 t/yr	Natural gas
Sleipner	Norway	Statoil	Operating > 1996	Offshore	900 m	Aquifer above	1 Mt/yr	Natural gas

## K12B-Offshore Netherlands (Gaz de France)



Figure 1: Field location map

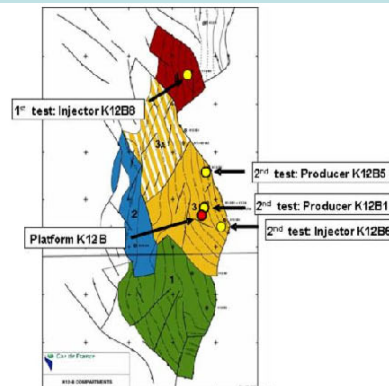
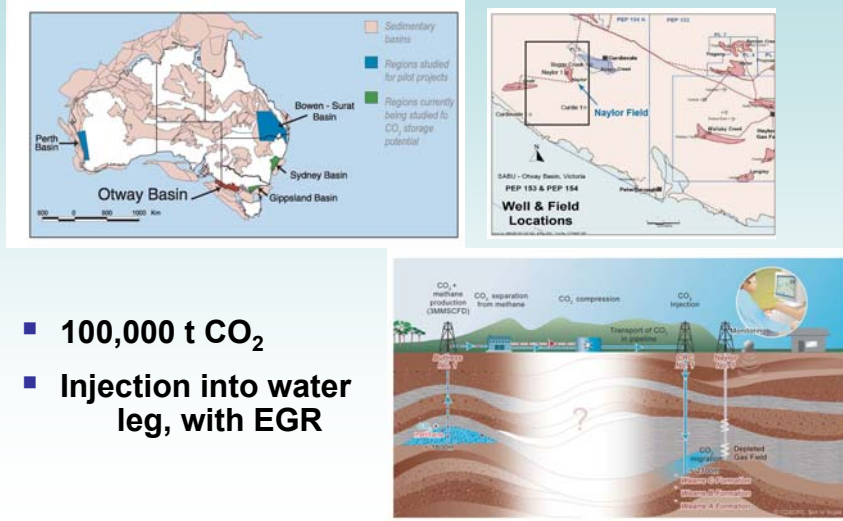


Figure 2: Schematic layout of the test locations.

- Phase 1. Feasibility of capture and injection
- Phase 2. Injection of separated CO<sub>2</sub>.
  - Test 1. Injection into isolated compartment
  - Test 2. Injection into producing gas reservoir (30,000 t/yr)
- Phase 3. Injection into gas reservoir at up to 475,000 t/yr

## Otway Basin Pilot, Australia



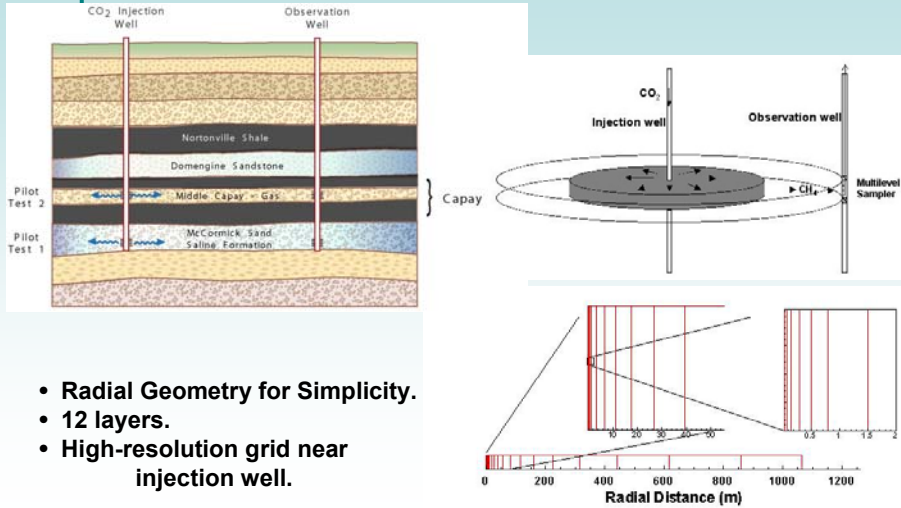
- 100,000 t CO<sub>2</sub>
- Injection into water leg, with EGR

Figure 5. Conceptual representations of the Otway Basin Pilot Project.

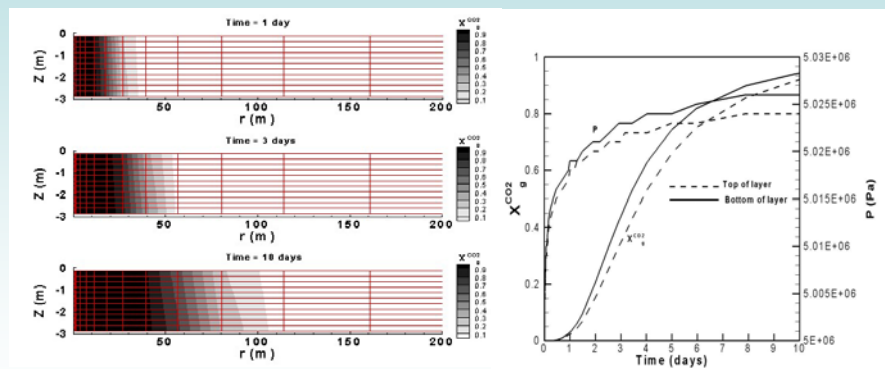
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## Rosetta Resources Pilot, Thornton CA



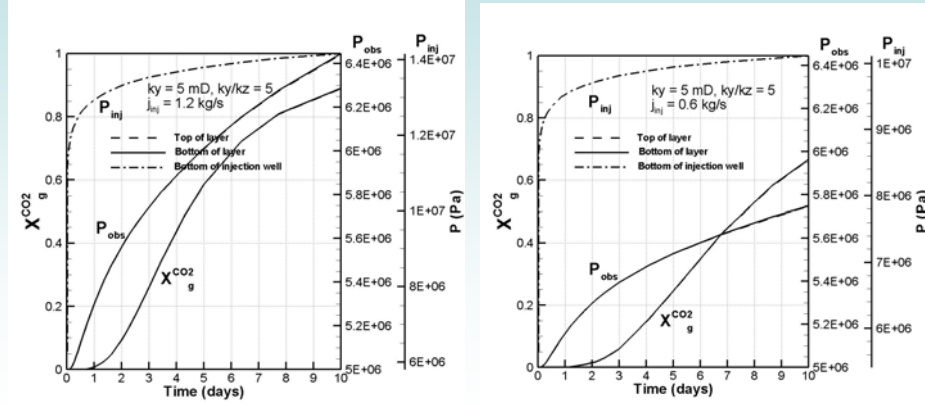
## Results for Capay



Breakthrough occurs after 1-2 days of injection.

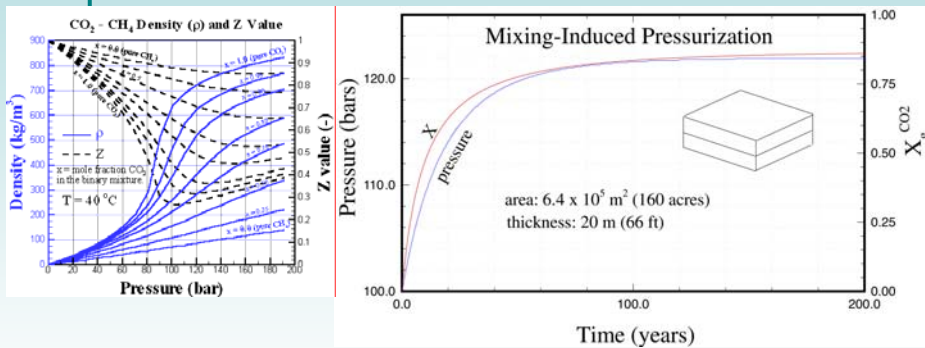
## Results for Capay

$k = 5 \text{ mD}$   
Two different injection rates  
Obs. well is at  $r = 39 \text{ m}$



Breakthrough occurs after 1-2 days of injection.

## Pressurization Due to Mixing



Supercritical  $\text{CO}_2$  and  $\text{CH}_4$  will eventually mix in the reservoir.

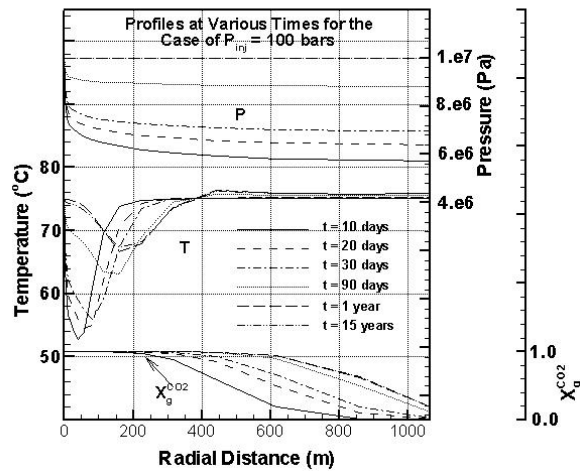
Pressure rises after injection stops due to compositional effect on  $\text{CO}_2$  density.

(see Oldenburg, Geological  $\text{CO}_2$  sequestration:  $\text{CO}_2$  transport in depleted gas reservoirs, in Ho and Webb, eds., *Gas Transport in Porous Media (Theory and Applications of Transport in Porous Media)*, Springer, 2006)

## J-T Cooling for High-Pressure Injection

Table 2. Properties of the 1-D radial gas reservoir.

Property	Value	Alt. Units
Radius	1130 m	0.70 mi
Thickness	50 m	164 ft
Porosity	0.30	0.30
Permeability	$10^{12} \text{ m}^2$	1 Darcy
Residual liquid saturation	0.2	0.2
Rock density ( $\rho_R$ )	$2600 \text{ kg m}^{-3}$	-
Rock heat capacity ( $C_R$ )	$1000 \text{ J kg}^{-1} \text{ }^\circ\text{C}^{-1}$	-
Formation thermal conductivity	$2.51 \text{ J m}^{-1} \text{ }^\circ\text{C}^{-1}$	-
Relative Permeability	Liquid: immob. Gas: unity	Liquid: 0. Gas: 1.
Molec. diffusivity (1 bar, 0 °C)	Liquid: $10^{15} \text{ m}^2 \text{ s}^{-1}$ Gas: $10^5 \text{ m}^2 \text{ s}^{-1}$	-
$T$ at $t = 0$	$75 \text{ }^\circ\text{C}$	$167 \text{ }^\circ\text{F}$
$P$ at $t = 0$	50 bars	725 psi
$P_{inj}$	100 bars $\text{CO}_2$	1470 psi
$\text{CH}_4$ production rate	$0.0 \text{ kg s}^{-1}$	0.0 Mcf/day
Final reservoir pressure after 15 yrs (high-P inj. case)	100 bars	1470 psi



Joule-Thomson cooling causes ~20 °C cooling near injection well.



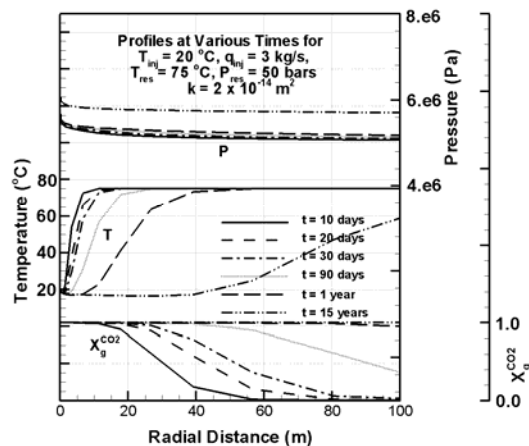
WEST COAST REGIONAL CARBON SEQUESTRATION PARTNERSHIP



## J-T Cooling for Constant-Rate Injection

Table 2. Properties of the 1-D radial gas reservoir.

Property	Value	Alt. Units
Radius	1130 m	0.70 mi
Thickness	50 m	164 ft
Porosity	0.30	0.30
Permeability	$10^{12} \text{ m}^2$ (base case) $2 \times 10^{15} \text{ m}^2$ (low-k case)	1 Darcy 20 mD
Residual liquid saturation	0.2	0.2
Rock density ( $\rho_R$ )	$2600 \text{ kg m}^{-3}$	-
Rock heat capacity ( $C_R$ )	$1000 \text{ J kg}^{-1} \text{ }^\circ\text{C}^{-1}$	-
Formation thermal conductivity	$2.51 \text{ J m}^{-1} \text{ }^\circ\text{C}^{-1}$	-
Relative Permeability	Liquid: immob. Gas: unity	Liquid: 0. Gas: 1.
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$T$ at $t = 0$	$75 \text{ }^\circ\text{C}$	$167 \text{ }^\circ\text{F}$
$P$ at $t = 0$	50 bars	725 psi
$\text{CO}_2$ injection rate	$3 \text{ kg s}^{-1}$	280 t/day
$T_{inj}$	$20 \text{ }^\circ\text{C}$	$68 \text{ }^\circ\text{F}$
$\text{CH}_4$ production rate	$0.56 \text{ kg s}^{-1}$	2514 Mcf/day
Final reservoir pressure after 15 yrs (base case)	55.6 bars	817 psi



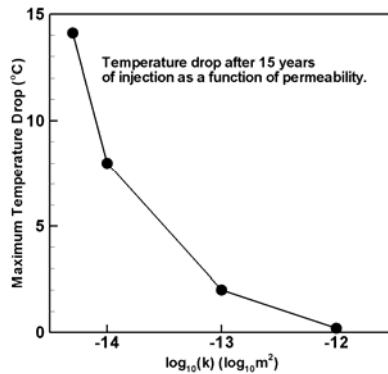
$k_{res} = 20 \text{ mD} \Rightarrow \text{small } \Delta P \Rightarrow \text{small } \Delta T.$



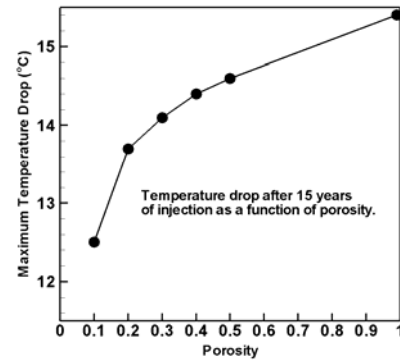
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## J-T Cooling Trends with $k$ and $\phi$



As  $k_{res}$  decreases  $\Rightarrow \Delta T$  increases.



As porosity increases  $\Rightarrow \Delta T$  increases.



## Summary

- CO<sub>2</sub> injection into gas reservoirs is the focus of pilot tests world-wide, but only a few involve EGR
- Pilot tests will answer key questions for CSEGR
  - Density effects (gravity override)
  - Mixing and early breakthrough
  - Injectivity (halite formation, hydrate formation)
  - Pressurization due to mixing
- Rosetta Resources Pilot
  - Reservoir is too thin to observe gravity override
  - Useful for mixing, breakthrough, injectivity, pressurization
- Results of the Rosetta Resources Pilot will be of world-wide interest



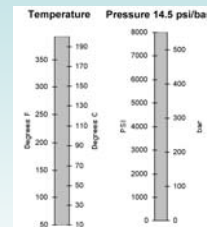
## Acknowledgments

This work was supported in part by WESTCARB through the Assistant Secretary for Fossil Energy, Office of Coal and Power Systems, through the National Energy Technologies Laboratory (NETL), and by Lawrence Berkeley National Laboratory under Department of Energy Contract No. DE-AC03-76SF00098 .



## Handy Conversions

- Standard conds. in U.S. are 14.7 psia, 60 F (~1 bar, 15.5 C)
- 1 MMBtu ≈ 1 Mcf CH<sub>4</sub>
- 1 Mcf = 10<sup>3</sup> cf = 28 m<sup>3</sup>
- 1 Mcf = 19 kg CH<sub>4</sub> at (1 bar, 15.5 C)
- 1 Mcf = 1.96 x 10<sup>3</sup> kg CH<sub>4</sub> at (100 bar, 40 C)
- 1 Mcf = 53 kg CO<sub>2</sub> at (1 bar, 15.5 C)
- 1 Mcf = 1.77 x 10<sup>4</sup> kg CO<sub>2</sub> (100 bar, 40 C)
- 1 tonne CO<sub>2</sub> = 10<sup>3</sup> kg = 18.8 Mcf = 526 m<sup>3</sup> (1 bar, 15.5 C)
- 1 tonne CO<sub>2</sub> = 10<sup>3</sup> kg = 0.056 Mcf = 1.58 m<sup>3</sup> (100 bar, 40 C)



### Density

$\rho_{\text{CH}_4}$  (1 bar, 15.5 C) = 0.68 kg/m<sup>3</sup>  
 $\rho_{\text{CH}_4}$  (100 bar, 40 C) = 70.0 kg/m<sup>3</sup>  
 $\rho_{\text{CO}_2}$  (1 bar, 15.5 C) = 1.9 kg/m<sup>3</sup>  
 $\rho_{\text{CO}_2}$  (100 bar, 40 C) = 632 kg/m<sup>3</sup>

### Viscosity

1 poise = 100 cp = 0.1 Pa s = 0.1 kg/(m s)  
 $\mu_{\text{H}_2\text{O}}$  = 1 cp = 10<sup>-3</sup> Pa s  
 $\mu_{\text{CH}_4}$  = 1.4 x 10<sup>-5</sup> Pa s (100 bar, 40 C)  
 $\mu_{\text{CO}_2}$  = 5.0 x 10<sup>-5</sup> Pa s (100 bar, 40 C)